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Bezeichnung der Erfindung/Title of the invention/Titre de l'invention:  
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If no title is shown please refer to the description.  
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Method for removing volatile components from polymer compositions

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**TITLE:****"METHOD FOR REMOVING VOLATILE COMPONENTS FROM POLYMER COMPOSITIONS"**

The present invention relates to the removal of volatile components from a polymeric composition. In particular, the present invention relates to a method for preparing butene-1 polymers having a low content of monomer by melt devolatilization of a polymeric solution obtained by liquid-phase polymerization of butene-1.

Butene-1 (co)polymers are well known in the art and are mainly used in the manufacture of molded products such as pipes, packaging films, adhesives.

Hitherto, butene-1 (co)polymers have been mainly produced by solution polymerisation and slurry polymerisation in the presence of coordination catalysts which are generally referred to as Ziegler-Natta catalysts. When a solution process is adopted, the polymerisation is preferably carried out in liquid butene-1 at conditions under which a solution of polybutene in butene-1 is discharged from the polymerisation reactor. When a slurry polymerisation is adopted, the polymerisation is carried out in liquid butene-1 at conditions under which the polymer is produced as a solid, thus obtaining a slurry of solid polymer in butene-1. In both cases, an additional step is required wherein the unreacted monomer is removed from the obtained polybutene-1.

In the art of the removal of volatile components from a polymerization fluid composition there are a number of well-known methods for reducing the volatile content of the resulting polymer composition as much as possible. These methods are mostly used for the continuous removal of volatile components from vinyl aromatic- or styrene-based polymers and involve heating the polymerization fluid composition containing volatile components to high temperatures, in the range of 150-250°C, and then flashing it in a devolatilization chamber. The extent of separation can be improved by raising the temperature at which the polymeric composition is introduced inside the devolatilization chamber or, in alternative, by decreasing the pressure in the volatilizer up to vacuum conditions.

Both the methods cannot be exploited to the fullest extent. On the one hand, as the temperature of the polymerization fluid composition is raised, the residual monomers can polymerize. The further and uncontrolled polymerisation that can take place during the

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heating phase would lead to an undesired modification of the final properties of the obtained polymer pellets. Moreover, the temperature must not exceed the limit at which phenomena of thermal degradation of the polymer chains occur.

On the other hand, enhancement of the degree of vacuum in the devolatilization chamber involves a marked increase in the volume of the separated gas, causing a considerable growth of the pressure drop within the piping. As a consequence, in the monomer recovery section the diameter of pipes as well as the size of the condenser must be increased with a consequent growth of the construction costs. A high degree of vacuum also causes a lowering of the dew point of the monomer so that the condensation of the monomer along the recycle line must be operated at very low temperatures, and this brings about additional operating costs.

In view of the above limits, it is extremely difficult to reduce the content of the volatile components, such as unreacted monomers, solvents, chain-transfer agents in a polymer composition to a sufficiently low level. For this reason, the use of an extruder endowed with vent openings, placed at the outlet of the devolatilization chamber, was adopted with the aim of reducing the volatile components remaining in the polymer to the fullest extent. However, the additional use of a vented extruder causes an increase in equipment and power costs, resulting in increased production costs.

Another type of devolatilization known in the art is carried out by means of suitable stripping agents, such as steam,  $\text{CO}_2$ ,  $\text{N}_2$ , etc. As an example thereof, USP 5,380,822 discloses a process for reducing the amount of residual monomer, dimer, trimer and solvent to less than 500 parts per million in a polymer or a polymer blend containing less than 2% weight of such residual monomer. The process comprises (i) heating said polymer at a temperature from 200-270°C, (ii) injecting into said polymer an amount of water greater than the amount of residual monomer, dimer, trimer and solvent but less than 10% weight, (iii) passing said polymer through a flash chamber devolatilizer maintained at a temperature from 200-270°C and a pressure lower than 8 torr.

USP 5,691,445 relates to a process for reducing the amount of residual monomer and solvent to less than 300 parts per million in a polymer or polymer blend of vinyl aromatic monomers, the process being characterized in that the devolatilization is fostered by the injection into the polymer melt of a suitable amount of  $\text{CO}_2$ .

The methods disclosed in USP 5,380,822 and 5,691,445 are not applicable to a polymeric (FE6028-EP)

solution obtained from a liquid phase polymerization of butene-1. In fact, the above stripping agents are not easily separable from the unreacted monomer when butene-1 has to be recovered and recycled to the polymerization reactor. In fact, conventional distillation units are not sufficient to achieve an acceptable separation and molecular sieves must be provided in order to complete efficiently the separation. The use of molecular sieves increases the complexity of the process and the operative costs in the recovery section.

In view of the above drawbacks, it would be desirable to provide a method for continuously removing, with a high efficiency, the unreacted butene-1 contained in a polymeric solution obtained by liquid polymerization of butene-1.

The Applicant has surprisingly found that subjecting the solution of polybutene in butene-1 to particular heating and devolatilization conditions allows to achieve the above separation with a high efficiency, thus minimizing the content of butene-1 in the final polybutene-1 up to less than 100 ppm.

It is therefore an object of the present invention a method for continuously removing unreacted monomer, and optionally other volatile components, from a polymeric solution obtained by a liquid-phase (co)polymerization of butene-1, the method comprising the steps of:

- a) subjecting the solution of polybutene in butene-1 to heating and mixing conditions such that a two-phase mixture is formed consisting substantially of: (1) a polybutene melt containing entrapped butene-1 and (2) supercritical gaseous butene-1;
- b) subjecting the above mixture to a sequence of devolatilization steps operating at decreasing pressures and at temperatures comprised between 170 and 220°C.

Besides butene-1, other volatile components to be removed are for instance comonomers, dimers, inert hydrocarbons, catalyst components and catalyst deactivators.

The polymerization takes place in liquid phase in the presence or absence of an inert hydrocarbon solvent. Suitable solvents can be liquid hydrocarbons having 5 to 10 carbon atoms, such as pentane, hexane, heptane, octane, etc. Preferably liquid butene-1 is used as the reaction medium and the bulk polymerization leads to the formation of a single liquid phase comprising a solution of polybutene-1 in butene-1. In order to obtain the best performance of the catalyst together with a complete miscibility of monomer and

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polymer, the polymerization temperature is generally kept at a value comprised in the range of from 65 to 85°C while the pressure is generally comprised between 8 and 40 bar. As regards the comonomers, the polymerization can be carried out in the presence of up to 20% by weight based on butene-1 of another  $\alpha$ -olefin: suitable comonomers are, for instance, ethylene, propylene, pentene-1 and hexene-1.

It is preferred to carry out the polymerization under such conditions that the concentration of polybutene-1 in the reaction medium does not become unduly high, as otherwise the polymeric solution will become too viscous and difficult to stir and/or process. Therefore, the polymerization is preferably conducted in such a way that the concentration of polybutene-1 in butene-1 is comprised between 10 and 35% by weight, more preferably between 20 and 30% by weight. As a consequence, a large amount of unreacted monomer, comprised between 65 and 90% by weight, has to be removed in order to obtain final polybutenes-1 with a low content of entrapped monomer.

Before carrying out the method for removal of volatile components according to the present invention wherein high temperatures of about 170-220°C are involved, the solution of polybutene-1 (PB-1) in butene-1 is generally subjected to a deactivation step of the catalyst residues. This avoids a further uncontrolled polymerisation or a thermal degradation of the polymer in step a) and b) of the present invention. The deactivation can be achieved in one or more mixing tanks placed in series or, alternatively, in a single deactivation apparatus equipped with a sequence of more mixing stages. In the case of polymerization carried out in the presence of a Ziegler-Natta catalyst, any of the deactivating compounds known in the art can be employed. Suitable deactivating compound are the organic compounds having a boiling point higher than 150°C and at least a hydroxy group. In particular, the organic compounds characterized by a ratio between the molecular weight (MW) and the number of hydroxy groups (OH) comprised between 20 and 100. Examples of deactivating compounds satisfying the above requirements are propylenglycol, dipropylenglycol, glycerol.

As a consequence of the polymerization conditions, the polymeric solution fed to step a) is a highly-viscous polymeric solution of polybutene-1 in butene-1 with a temperature comprised between 65 and 85°C. The heating and mixing conditions of step a) must take into account the high viscosity, of about  $10^3$ - $10^5$  cP, of the solution to be treated. Furthermore, the operative conditions must be accurately selected in order to cause the

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passage from a single liquid phase, i.e. a solution of PB-1 in butene-1, to a two-phase mixture consisting substantially of (1) a polybutene melt containing entrapped butene-1 and (2) supercritical gaseous butene-1. The amount of butene-1 entrapped into the polybutene melt is generally less than 10% by weight, preferably less than 6% by wt. With the term of "polybutene-1 melt" is intended polybutene in the molten state; in spite of its very high viscosity (of about  $20 \times 10^6$  cP) is still able to flow as a fluid inside pipes and similar. In view of the particular polybutene/butene-1 phase equilibrium, the following conditions are important in carrying out the transformation of step a):

(I) The separation of partially-solid polymer should be accurately prevented during step a) in order to avoid the clogging of the apparatus employed to carry out the mixing and heating conditions of step a). In fact, a partially-solid polymer obstructs the flowability into the apparatus: even if re-molten by the high temperatures adopted in step a), a continuous solidification and re-melting of the polymer causes an unstable working of the apparatus and unexpected fluctuations of temperature and pressure. The Applicant has found that this drawback can be avoided by feeding the polymeric solution to the heating step a) at a pressure of not less than 22 bar, preferably in the range of from 25 to 80 bar. A pump for high viscosity fluids, such as a gear pump or a screw pump, can be placed on the line connecting the polymerization reactor to the heating and mixing step a) in order to provide the polymeric solution with the requested value of pressure.

(II) The temperature of the two-phase mixture obtained at the outlet of step a) should suitably be set at values such to substantially avoid during step b) the following drawbacks: a thermal degradation of the polymer chains due to high temperature and/or the separation of a polybutene melt excessively viscous which cannot prime any pump. In order to satisfy the above requirement, the temperature of the two-phase mixture obtained from step a) and fed to the sequence of devolatilization steps b) is set in the range from 170 to 220°C.

According to a preferred embodiment, the heating and mixing conditions of step a) are preferably obtained by flowing the solution of polybutene in butene-1 through a multi-tube heat exchanger wherein static mixing elements are inserted inside each tube. The presence of a plurality of static mixing elements inside each tube is aimed to achieve an intense mixing of the highly-viscous solution and to prevent channeling. In fact, said elements cause mixing between the outermost and the innermost veins of the flowing

stream so favoring a good heat transfer between the different threads of fluid. As a consequence, a two-phase mixture having a homogenous distribution of temperature is obtained at the outlet of the step a). Preferably, mixing rods are used as static elements inserted in the tubes of the heat exchanger. Within each tube they cause splitting of the flowing stream, changing of the direction of flow and joining of the split streams.

The mixture formed in step a) is passed to step b), carried out in a sequence of devolatilization steps operating at decreasing pressures. According to a preferred embodiment of the invention, step b) comprises two successive devolatilization chambers or volatilizers placed in series, the first one operating at a pressure higher than the atmospheric pressure, the second one operating under vacuum. This particular embodiment allows to achieve a remarkable reduction of the content of butene-1 in the final polybutene pellets.

The two-phase mixture is introduced at the top of a first empty volatilizer, operated at a temperature of from 170 to 220°C and at a pressure of from 2 to 12 bar. In said first volatilizer, the components of the mixture formed in step a) are separated by gravity: the polymer melt pours downwards while the supercritical gas flows upward. During the vertical drop of the polymer melt along the chamber a further amount of butene-1 is released away so that at the outlet of the first volatilizer the content of butene-1 in the polybutene melt is generally reduced to less than 5% by weight. The supercritical gas collected at the top of the first volatilizer can contain a little amount of other volatile components, such as inert hydrocarbons, catalyst deactivators, etc so that the monomer recovery requires the separation of said compounds from butene-1. This separation step comprises one or more distillation columns, a drying unit and the recycle of liquid butene-1 to the polymerization section.

The polybutene-1 melt coming out of the first volatilizer is introduced into a second devolatilization chamber, operated in the same range of temperature of the first volatilizer but at a pressure comprised between 5 and 100 mbar. As a consequence of said vacuum conditions a further amount of butene-1 is released away during the drop and settling of the PB-1 melt inside the volatilizer. At the outlet of the second volatilizer the content of butene-1 in the polybutene melt is strongly reduced, obtaining an amount of butene-1 up to less than 100 ppm weight.

Along the line connecting the first volatilizer to the second one, a partial cooling of the  
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polymer melt can occur, so that at the outlet of the first volatilizer the polybutene-1 melt is preferably introduced into a second multi-tube heat exchanger. This heat exchanger has the function of adjusting the temperature of the polymer melt up to the value requested in the second devolatilization chamber.

The obtained polybutene-1 melt is characterized by a very high viscosity, of about  $20 \times 10^6$  cP. As a consequence, specific pumps, such as gear pumps, are preferably used to guarantee the extraction of the melt from the bottom of each devolatilization chamber. Preferably, the gear pump is directly coupled to the bottom flange of each volatilizer in order to prime the pump and so to convey the PB-1 melt to the following process steps.

The method of the present invention is characterized by an excellent efficiency in the removal of unreacted butene-1 from butene-1 polymers, so that the following and other advantages can be achieved by the present invention:

- the minimization of the content of butene-1 at such low values dramatically reduces the problems of explosiveness due to the release of butene-1 incorporated in the final pellets. In fact, a considerable presence of monomer requires a massive and long-period ventilation of the pellets during the storage thereof to reduce the risks of explosiveness; the minimization of butene-1 content at values lower than 100 ppm allows to avoid said forced ventilation of the pellets during the storage thereof;
- the use of a vented extruder, commonly adopted in some prior art processes, is avoided in the method of the invention, advantageously replaced by a simpler and cheaper apparatus, such as a static mixer.

A static mixer placed downstream the last volatilizer can therefore be used in the present invention to carry out the mixing of the polymer melt with the suitable additives, such as antioxidant compounds, nucleating agents, pigments, etc.

A side-arm extruder serves to melt and convey the masterbatch, a pre-compounded concentrate of the final product additives package, into the static mixer wherein an intimate mixing of the additives with the polybutene melt is achieved.

The polymer exiting the static mixer is conveyed to an underwater pelletizer where is cut into pellets by the action of rotating knife blades and immediately cooled by means of chilled water.

As said, the method of the present invention is generally indicated for the removal of volatile components contained in a polymeric solution obtained by a liquid-phase process

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for homo- or copolymerizing butene-1.

It is therefore another object of the present invention a liquid-phase process for homo- or copolymerizing butene-1, comprising a liquid phase polymerization of butene-1 in the presence of a catalyst based on a transition metal compound and the method for the removal of volatile components contained in a solution of polybutene-1 in butene above described.

A preferred embodiment of the method of the invention is described in detail with reference to the accompanying Figure 1.

A solution of PB-1 in butene-1 withdrawn from the polymerization section is fed via line 1 to a deactivation pot 20 for the deactivation of the catalyst residues. A gear pump 30 is placed on line 2 to introduce the polymer solution into a multi-tube heat exchanger 40 where the heating and mixing conditions of step a) of the present invention are carried out. The two-phase mixture obtained at the outlet of the heat exchanger 40 is passed via line 3 to a first devolatilization chamber 50.

The two components of the mixture are separated by gravity into the volatilizer 50: the polymer melt pours downwards and collects at the bottom of the volatilizer, while the supercritical gaseous monomer flows upward. The gas collected at the top of the volatilizer 50 is passed via line 4 to the monomer recovery section and then returned as liquid butene-1 to the polymerization section via line 5.

The polybutene-1 melt is withdrawn by means of a gear pump 60 from the bottom of the first volatilizer 50 and introduced into a second multi-tube heat exchanger 70 via line 6. Afterwards, the PB-1 melt is fed via line 6 at the top of a second volatilizer 80 wherein vacuum conditions are caused by the action of a vacuum pump 120 placed on line 7. The gaseous butene-1 collected at the top of the second volatilizer 80 is sent via line 7 to the recovery section. The polybutene-1 melt withdrawn by means of a gear pump 90 from the bottom of the second volatilizer 80 is introduced into a static mixer 100 via line 10. A side-arm extruder 110 is used for melting and mixing the additives used for the compounding of the polymer; said additives are fed via line 8, while line 9 connects the side-arm extruder 110 to the static mixer. The polymer melt exiting the static mixer 100 is then passed to an underwater pelletizer where it is cut into pellets.

The following examples have to be considered representative and non-limiting of the scope of the invention.

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## EXAMPLES

The following examples relate to some tests carried out in a pilot plant and aimed at evaluating the effectiveness of the claimed method to remove continuously unreacted butene-1 from a solution of polybutene-1 (PB-1) in butene-1.

The polymer solution was obtained by a liquid-phase polymerization carried out into two continuously stirred tank reactors having a volume of 0,33 m<sup>3</sup>. Liquid butene-1 was used as the reaction medium and the polymerization conditions were selected as follows: T=75°C, p=18 bar.

### Example 1

A highly-viscous solution of polybutene-1 in butene-1 with a polymer concentration of 25% by wt and a polymer melt index of 0,40 was treated according to the embodiment of Fig.1 of the present invention.

The polymer solution withdrawn from the polymerization reactor was passed through a gear pump in order to increase its pressure to a value of 30 bar. Then, the solution of PB-1 in butene-1 was subjected to heating and mixing conditions according to step a) of the invention by flowing it through a multi-tube heat exchanger. The length of this apparatus was 1,2 m, the number of tubes was 60, the diameter thereof was 20 mm. Mixing rods were used as mixing elements inside each tube.

A diathermic oil (MARLOTHERM N) was fed at 260°C into the heat exchanger as a heating fluid. At the outlet of the heat exchanger a mixture was obtained consisting of: (1) a polybutene-1 melt containing 3,6% by weight of butene-1 and (2) gaseous butene-1. The operative conditions at the outlet of the multi-tube heat exchanger were the following: T=210°C, p=7 bar.

The same operative conditions were adopted in the first devolatilization chamber wherein the above mixture was introduced: due to the gravity, the polybutene melt was collected at the bottom of the chamber, while the gaseous butene-1 flowed upward. At the outlet of this volatilizer the content of butene-1 in the polybutene melt was checked: a value of 1,9% by weight was measured.

The PB-1 melt was withdrawn from the bottom of the first volatilizer by means of a gear pump and then introduced into a second multi-tube heat exchanger wherein the polymer melt was heated up to the temperature requested into the second devolatilization (FE6028-EP)

chamber.

The second devolatilization chamber was operated under vacuum at 210°C and 25 mbar. At the outlet of this second volatilizer the content of monomer in the polybutene melt was measured obtaining a value of only 67 ppm weight.

A static mixer placed downstream the second devolatilization chamber was used to mix the polymer melt with Irganox 1010 as an antioxidant compound, talc as a nucleating agent, carbon black and  $\text{TiO}_2$  as pigments. A side-arm extruder was used to melt and convey the additives into the static mixer. Finally, the additivated polybutene melt exiting the static mixer was conveyed to an underwater pelletizer to be cut into pellets.

#### Example 2

A solution of a butene-1 random copolymer (containing 5,8% by wt of ethylene) having a polymer concentration of 25% by wt and a melt index of 2,2 was treated according to the present invention.

The polymer solution withdrawn from the polymerization reactor was passed through a gear pump in order to increase its pressure to a value of 27 bar. Then, the solution of PB-1 in butene-1 was passed through the same multi-tube heat exchanger of example 1.

At the outlet of the heat exchanger a mixture was obtained consisting of: (1) a polybutene-1 melt containing 3,8% by weight of butene-1 and (2) gaseous butene-1. The operative conditions at the outlet of the multi-tube heat exchanger were the following:  $T=190^\circ\text{C}$ ,  $p=6$  bar. The same operative conditions were adopted in the first devolatilization chamber wherein the above mixture was introduced: due to the gravity, the polybutene melt was collected at the bottom of the chamber, while the gaseous butene-1 flowed upward. At the outlet of this volatilizer the content of butene-1 in the polybutene melt was checked: a value of 1,9% by weight was measured. The PB-1 melt was withdrawn from the bottom of the first volatilizer by means of a gear pump and then introduced into a second multi-tube heat exchanger wherein the polymer melt was heated up to the temperature requested into the second devolatilization chamber.

The second devolatilization chamber was operated under vacuum at 190°C and 20 mbar. At the outlet of this second volatilizer the content of monomer in the polybutene melt was measured obtaining a value of only 64 ppm weight.

The polybutene-1 melt was compounded into a static mixer as in example 1. Finally, the additivated polybutene melt was conveyed to an underwater pelletizer to be cut into

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pellets.

### Example 3

A solution of polybutene-1 in butene-1 having a concentration of 30% by wt and a melt index of 20,0 was treated according to the present invention.

The polymer solution withdrawn from the polymerization reactor was passed through a gear pump in order to increase its pressure to a value of 25 bar. Then, the solution of PB-1 in butene-1 was passed through the same multi-tube heat exchanger of example 1.

At the outlet of the heat exchanger a mixture was obtained consisting of: (1) a polybutene-1 melt containing 3,5% by weight of butene-1 and (2) gaseous butene-1. The operative conditions at the outlet of the multi-tube heat exchanger were the following:  $T=180^{\circ}\text{C}$ ,  $p=5$  bar. The same operative conditions were adopted in the first devolatilization chamber wherein the above mixture was introduced: due to the gravity, the polybutene melt was collected at the bottom of the chamber, while the gaseous butene-1 flowed upward. At the outlet of this volatilizer the content of butene-1 in the polybutene melt was checked: a value of 1,7% by weight was measured.

The PB-1 melt was withdrawn from the bottom of the first volatilizer by means of a gear pump and then introduced into a second multi-tube heat exchanger wherein the polymer melt was heated up to the temperature requested into the second devolatilization chamber.

The second devolatilization chamber was operated under vacuum at  $180^{\circ}\text{C}$  and 10 mbar. At the outlet of this second volatilizer the content of monomer in the polybutene melt was measured obtaining a value of only 35 ppm weight.

The polybutene-1 melt was compounded in a static mixer as in example 1. Finally, the additivated polybutene-1 melt was conveyed to an underwater pelletizer to be cut into pellets.

### Example 4

The same solution of polybutene-1 in butene-1 of the example 1 (polymer concentration 25% by wt, melt index of 0,40) was passed through a gear pump in order to increase its pressure to a value of 30 bar. Then, the solution of PB-1 in butene-1 was passed through the same multi-tube heat exchanger of example 1.

At the outlet of the heat exchanger a mixture was obtained consisting of: (1) a polybutene-1 melt containing 3,8% by weight of butene-1 and (2) gaseous butene-1. The

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operative conditions at the outlet of the multi-tube heat exchanger were the following:  $T=210^{\circ}\text{C}$ ,  $p=7$  bar. The same operative conditions were adopted in the first devolatilization chamber wherein the above mixture was introduced: the polybutene melt was collected at the bottom of the chamber, while the gaseous butene-1 flowed upward. At the outlet of this volatilizer the content of butene-1 in the polybutene melt was checked: a value of 1,9% by weight was measured.

The second devolatilization chamber was operated under vacuum at  $210^{\circ}\text{C}$  and 200 mbar. At the outlet of this second volatilizer the content of monomer in the polybutene melt was measured obtaining a value of 540 ppm weight.

#### Example 5 (comp.)

The same solution of polybutene-1 in butene-1 of the example 1 (polymer concentration 25% by wt, melt index of 0,40) was introduced into the multi-tube heat exchanger of example 1 at the following conditions:  $T=75^{\circ}\text{C}$ ,  $p=18$  bar.

It was observed an unstable working of the heat exchanger due to uncontrolled and unexpected fluctuations of temperature and pressure. The separation inside the apparatus of a partially-solid polymer, in addition to the two-phase mixture (PB-1 melt and gaseous butene-1), interfered with the flowability of the two-phase mixture. The formation of cold spots was so remarkable that at the outlet of the heat exchanger the obtained mixture was not stable as regards concentration, temperature and pressure.

#### Example 6 (comp.)

The same solution of polybutene-1 in butene-1 of the example 3 (polymer concentration 30% by wt, melt index of 20,0) was passed through a gear pump in order to increase its pressure to a value of 25 bar. Then, the solution of PB-1 in butene-1 was passed through the same multi-tube heat exchanger of example 1.

At the outlet of the heat exchanger a mixture was obtained consisting of: (1) a polybutene-1 melt containing 4,2% by weight of butene-1 and (2) supercritical gaseous butene-1. The operative conditions at the outlet of the multi-tube heat exchanger were the following:  $T=160^{\circ}\text{C}$ ,  $p=5$  bar. The above mixture was introduced into the first devolatilization chamber: it was observed that due to the excessive viscosity of the melt separated at the bottom of the chamber, it was not possible to prime the gear pump and to transfer the melt to the successive steps. This example proves that when the temperature of the two-phase mixture fed to step b) is under the claimed range, the method of the

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invention cannot be carried out.

**CLAIMS**

1. A method for continuously removing the unreacted butene-1, and optionally other volatile components, from a polymeric solution obtained by liquid phase (co)polymerization of butene-1, the method comprising the steps of:
  - a) subjecting the polymeric solution to heating and mixing conditions such that a mixture is formed consisting substantially of: (1) a polybutene melt containing entrapped butene-1 and (2) supercritical gaseous butene-1;
  - b) subjecting the above mixture to a sequence of devolatilisation steps operating at decreasing pressures and at temperatures comprised between 170 and 220°C.
2. The method according to claim 1 wherein the other volatile components are comonomers, dimers, inert hydrocarbons, catalyst components and catalyst deactivators.
3. The method according to claim 1 wherein the polymeric solution obtained by liquid phase (co)polymerization of butene-1 is a solution of polybutene-1 in butene-1 containing unreacted butene-1 in a percentage comprised between 65 and 90% by weight.
4. The method according to claim 1 wherein the polymeric solution is fed to step a) at a temperature of 65-85°C.
5. The method according to claim 1 wherein the polymeric solution is fed to step a) at a pressure of at least 22 bar.
6. The method according to claim 5, wherein the polymeric solution is fed to step a) at a pressure in the range of from 25 to 80 bar.
7. The method according to claim 1 wherein the heating and mixing conditions of step a) are obtained by flowing the solution of polybutene in butene-1 through a multi-tube heat exchanger wherein static mixing elements are inserted inside each tube.
8. The method according to claim 7 wherein the static mixing elements are mixing rods.
9. The method according to claim 1 wherein the amount of butene-1 entrapped into the polybutene melt is less than 10% by wt.
10. The method according to claim 1 wherein the amount of butene-1 entrapped into

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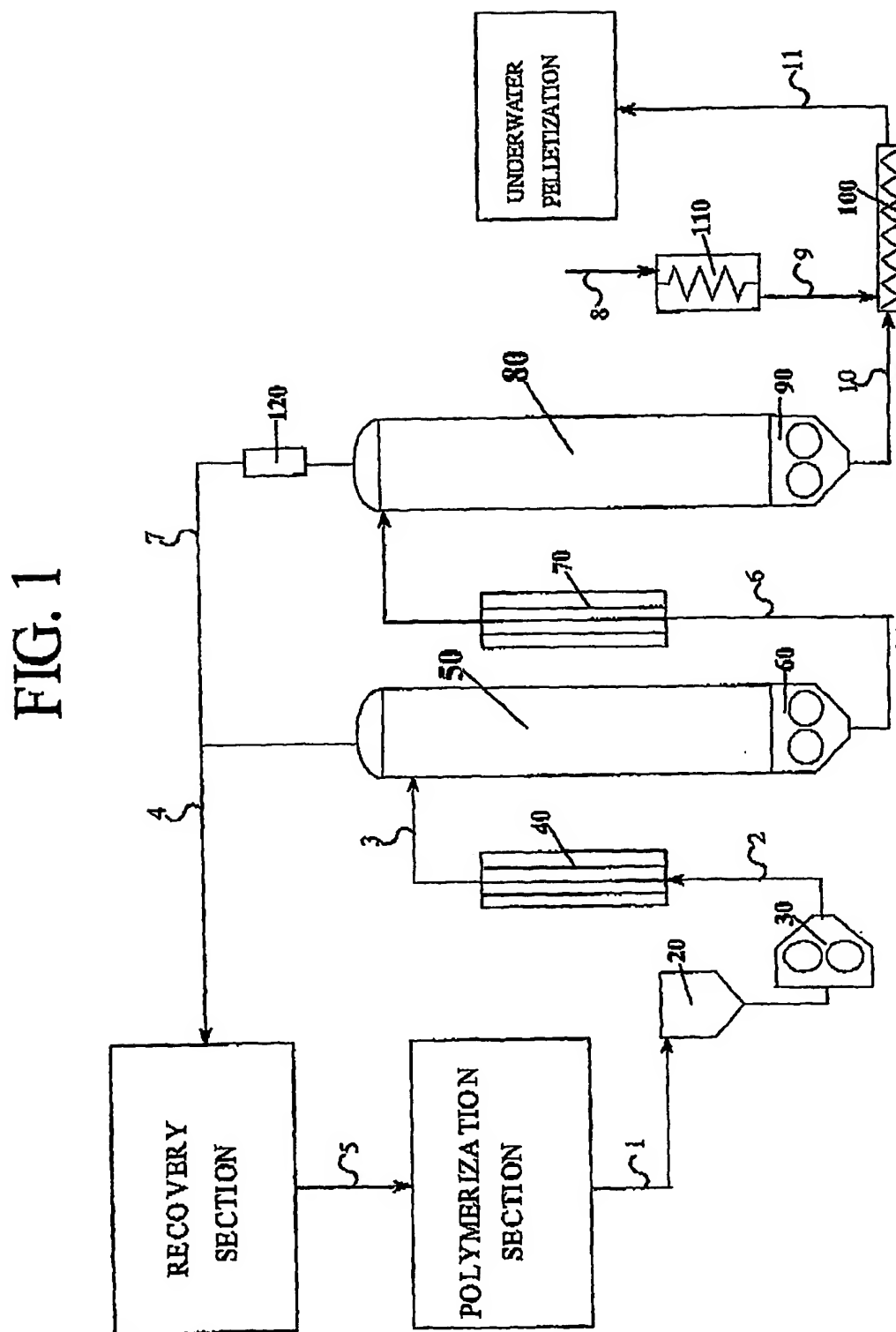
the polybutene melt is less than 6% by wt.

- 11 The method according to claim 1 wherein step b) comprises two successive volatilizers placed in series, the first one operating at a pressure higher than the atmospheric pressure, the second one operating under vacuum.
- 12 The method according to claim 11 wherein the first volatilizer is operated at a temperature of from 170 to 220°C at a pressure of from 2 to 12 bar.
- 13 The method according to claim 12 wherein at the outlet of the first volatilizer the content of butene-1 in the polybutene melt is reduced at less than 5% by weight.
- 14 The method according to claims 1-13 wherein the polybutene melt coming from the first volatilizer is introduced into a second volatilizer operated at a temperature of from 170 to 220°C at a pressure of from 5 to 100 mbar.
- 15 The method according to claim 14 wherein at the outlet of the second volatilizer the content of butene-1 in the polybutene melt is reduced at less than 100 ppm.
- 16 The method according to claims 1-15 wherein a static mixer placed downstream the last volatilizer is used to carry out the compounding of the polymer melt.
- 17 A liquid-phase process for homo- or copolymerizing butene-1, comprising a liquid phase polymerization of butene-1 in the presence of a catalyst based on a transition metal compound and the method for the removal of volatile components according to claims 1-16.

**ABSTRACT**

Method for continuously removing the unreacted butene-1, and optionally other volatile components, from a polymeric solution obtained by liquid phase (co)polymerization of butene-1, the method comprising the steps of:

- subjecting the polymeric solution to heating and mixing conditions such that a mixture is formed consisting substantially of: (1) a polybutene melt containing entrapped butene-1 and (2) supercritical gaseous butene-1;
- subjecting the above mixture to a sequence of devolatilisation steps operating at decreasing pressures.



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